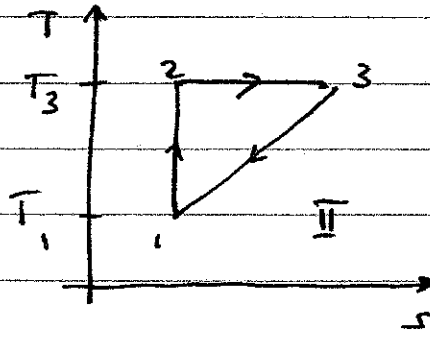
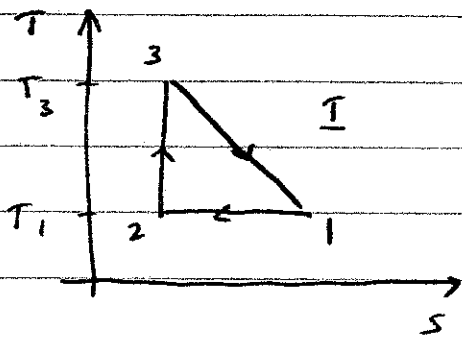


T1

16. Unified Sp09

Concepts: def. of entropy, thermal eff.

25



all processes  
internally reversible  
 $Tds = dq$

$$\eta_{th} = \frac{W_{net}}{q_A} = \frac{q_A + q_R}{q_A} \quad q \text{ is heat to system } (q_R < 0)$$

and  $q = \int T ds$

$$\eta_{th}^I = 1 + \frac{\int_2^3 T ds}{\int_1^3 T ds} = 1 + \frac{\bar{T}_{12} (s_2 - s_1)}{\bar{T}_{31} (s_1 - s_3)} = 1 - \frac{\bar{T}_{12}}{\bar{T}_{31}}$$

$$\eta_{th}^I = 1 - \frac{2T_1}{T_3 + T_1} \rightarrow \eta_{th}^I = \frac{T_3 - T_1}{T_2 + T_1}$$

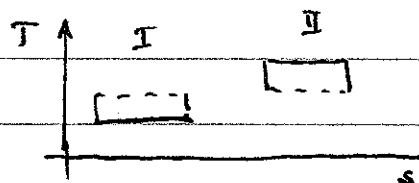
$$\eta_{th}^{II} = 1 + \frac{\int_3^1 T ds}{\int_2^3 T ds} = 1 + \frac{\bar{T}_{31} (s_1 - s_3)}{\bar{T}_{23} (s_3 - s_2)} = 1 - \frac{\bar{T}_{31}}{\bar{T}_{23}}$$

$$\eta_{th}^{II} = 1 - \frac{T_3 + T_1}{2T_2} \rightarrow \eta_{th}^{II} = \frac{T_3 - T_1}{2T_2}$$

$\eta_{th}^I > \eta_{th}^{II}$

because temperature ratio of heat sink to heat source (on average basis) lower for cycle I

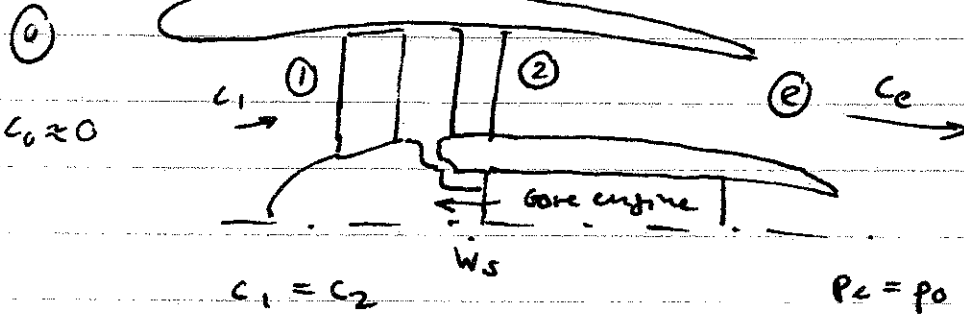
$$\frac{\bar{T}_R}{\bar{T}_A} \Big|_I < \frac{\bar{T}_R}{\bar{T}_A} \Big|_{II}$$



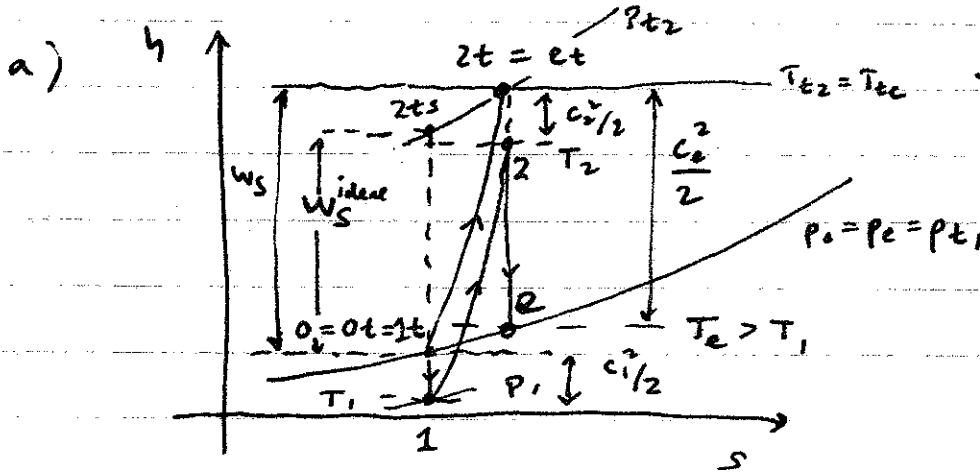
cannot:  
more "waste"  
heat in cycle II  
for same net  
work

T2 (h-s diagrams, Gibbs, integral man. equation)

16. Unified sp 09  
25



- Assume:
- adiabatic non-ideal fan,
  - core mass flow negligible



5) 1st Law CV enths:  $W_s = \dot{m}(h_{t2} - h_{t1})$

$h_{t1} = h_{t1}, h_{t2} = h_{t2}$

$\dot{m} = \frac{W_s}{c_p(T_{t2} - T_{t1})}$

$T_{t1} = T_{t0} = T_0 = 300K$

use adiab. eff to find  $T_{t2}$ :  $\eta_{fan} = \frac{W_s^{ideal}}{W_s} = \frac{T_{t2s} - T_{t1}}{T_{t2} - T_{t1}}, T_{t2s} = \left(\frac{p_{t2}}{p_{t1}}\right)^{\frac{\gamma-1}{\gamma}}$

so  $T_{t2} = T_{t1} \left(1 + \frac{1}{\eta_{fan}} \left[\left(\frac{p_{t2}}{p_{t1}}\right)^{\frac{\gamma-1}{\gamma}} - 1\right]\right); T_{t2} = 335.6K; \dot{m} = 699 kg/s$

c)  $T_{t2} = T_2 + \frac{c_2^2}{2c_p}, c_1 = c_2 = \sqrt{2c_p(T_0 - T_1)}, T_2 = T_{t2} - \frac{c_2^2}{2c_p} = 320.5K$

$c_1 = c_2 \rightarrow T_{t1} = T_0 = T_1 + \frac{c_1^2}{2c_p} \uparrow M_2 = \frac{c_2}{\sqrt{\gamma R T_2}} \quad M_2 = 0.485$

d) Gibbs:  $T ds = dh_t - v dp_t \int_1^2; s_2 - s_1 = c_p \ln\left(\frac{T_2}{T_1}\right) - R \ln\left(\frac{p_2}{p_1}\right)$

no other interaction:  $\Delta S_{tot} = \Delta S_{gen} = \Delta S_{fan} = s_2 - s_1, \Delta S_{gen} = 16.1 J/kg-K$  (ad. fan)

e) Integral man. eqn:

$T = \dot{m}(c_2 - c_1) = \dot{m}c_2$

$T = 173.7 KN \leftarrow$

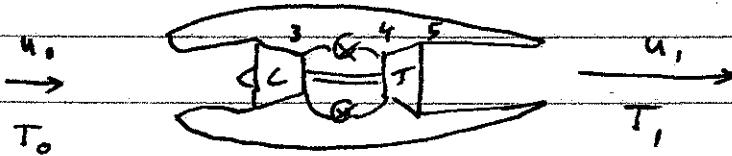
isentropic expansion in nozzle

$p_{t2} = p_{t2} = p_c \left(1 + \frac{\gamma-1}{2} M_2^2\right)^{\frac{\gamma}{\gamma-1}}, p_c = p_{t1}$

$M_2 = \sqrt{\left[\frac{p_{t2}}{p_{t1}}\right]^{\frac{\gamma-1}{\gamma}} - 1} = 0.71$

$T_c = T_{t2} \left(1 + \frac{\gamma-1}{2} M_2^2\right)^{-1} = 304.8K$

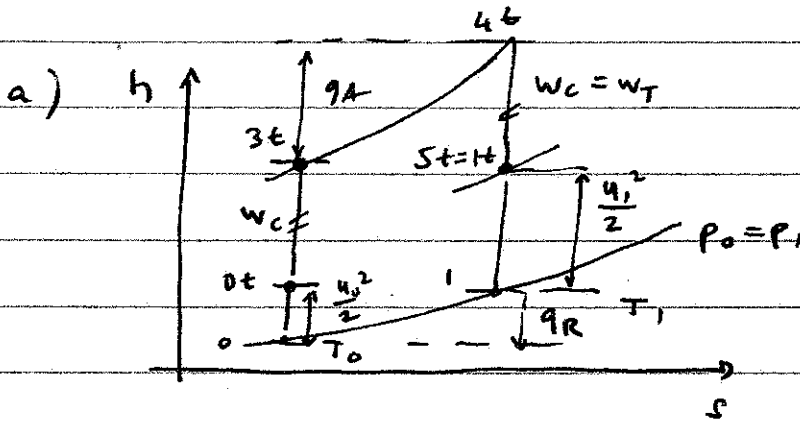
$c_c = M_2 \sqrt{\gamma R T_c}$   
 $c_c = 248.5 m/s$



know:  $u_0, u_1, T_0, T_1, c_p$

assume: ideal cycle  
steady level flight  
ideal gas,  $c_p = \text{const}$

Concepts: ideal Brayton cycle  
h-s diagrams  
overall, prop. eff.



b)  $q_R = c_p (T_1 - T_0)$  from 1st law

c)  $q_A - q_R = q_{net} = w_{net}$ ,  $w_{net} = \frac{u_1^2}{2} - \frac{u_0^2}{2}$ ;  $q_{net} = \frac{u_1^2}{2} - \frac{u_0^2}{2}$

d)  $\eta_{th} = \frac{w_{net}}{q_A} = \frac{w_{net}}{q_R + w_{net}} = \frac{1}{1 + q_R/w_{net}}$

$\eta_{th} = \left( 1 + \frac{2c_p (T_1 - T_0)}{u_1^2 - u_0^2} \right)^{-1}$

e)  $\eta_0 = \eta_{prop} \cdot \eta_{th}$ ;  $\eta_{prop} = \frac{\text{thrust power}}{\text{mech-power}} = \frac{u_1(u_1 - u_0)u_0}{u_1(\frac{u_1^2}{2} - \frac{u_0^2}{2})}$

$\eta_{prop} = \frac{2}{1 + \frac{u_1}{u_0}}$

$\eta_0 = \frac{2}{1 + u_1/u_0} \frac{(u_1^2 - u_0^2)}{u_1^2 - u_0^2 + 2c_p (T_1 - T_0)}$ ;  $\eta_0 = \frac{2u_0 \cdot (u_1 + u_0)}{u_1^2 - u_0^2 + 2c_p (T_1 - T_0)}$